

Reinhold Environmental Ltd.



2006 APC Round Table & Expo Presentation

July 16-18, 2006, Columbus, OH

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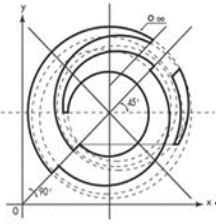


July 18, 2006

Overview of WESP's for Fine Particulate and H₂SO₄ Collection

Steve Francis

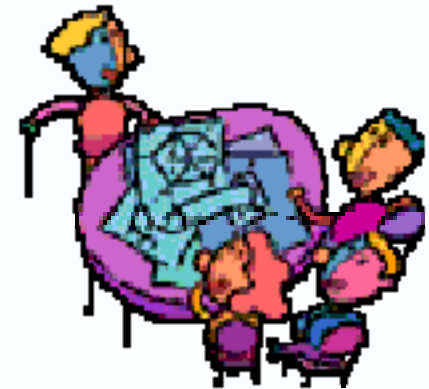
ALSTOM

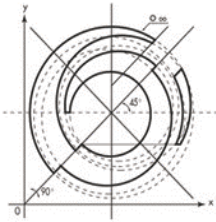


Agenda

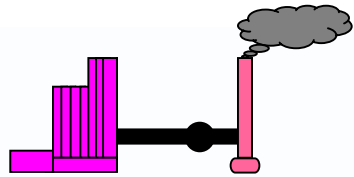


- Emissions Limitations
- SO_3 (H_2SO_4) Formation
- Reduction of SO_3 (H_2SO_4)
- WESP Designs
- WESP Arrangements
- WESP Wash Water Systems
- WESP Installation Details
- Summary & Conclusions

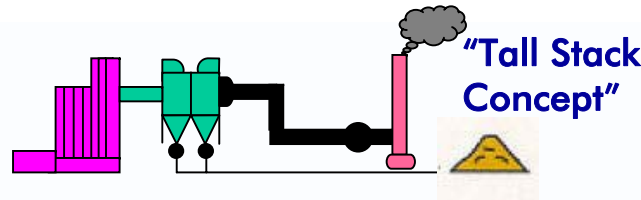




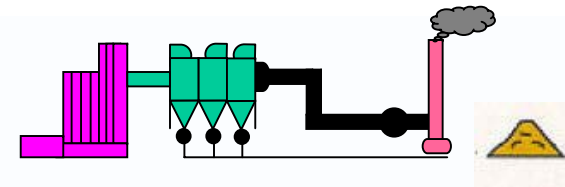
AIR POLLUTION CONTROL EVOLUTION



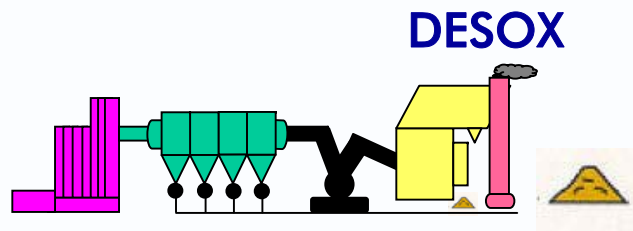
1950s



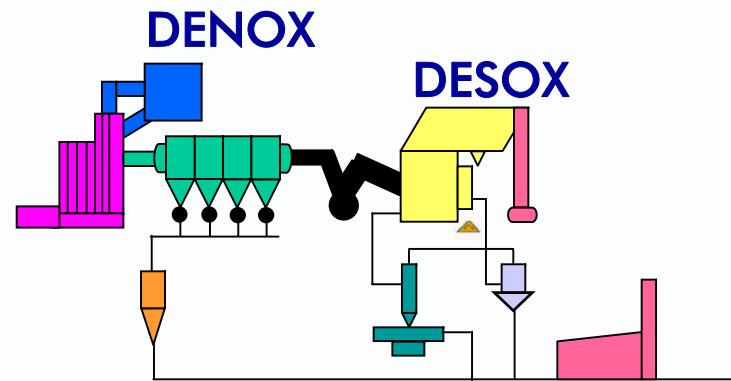
1960s



1970s

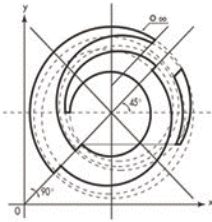


1980s



1990-Today End Product Recovery and Utilization

MASS & VISIBLE EMISSION LIMITS ARE BEING REDUCED

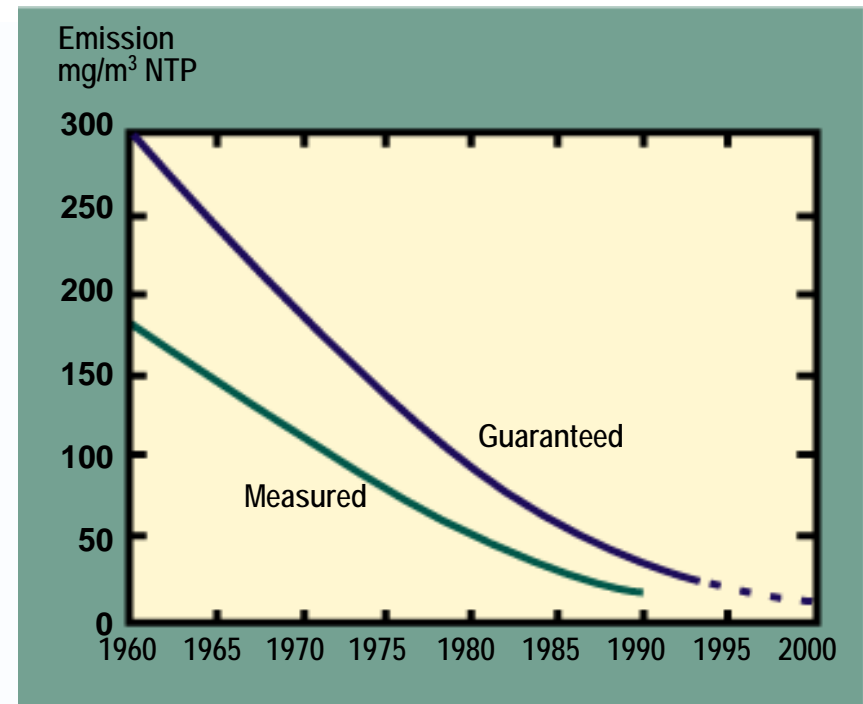


EMISSIONS REQUIREMENTS

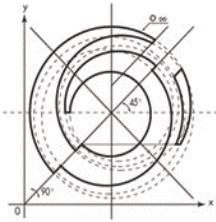


Trends:

- Guarantees Are Now As Low As 10 mg/Nm^3 (0.005 gr/SCF)
- Trend Toward 5 mg/Nm^3 (0.0025 gr/SCF)
- Increased Emphasis on Removal of Fine Particles (PM 2.5)
- Particulate Emissions Including Condensibles
- More and More Emphasis on Removal of Mercury and HAP's



TREND TOWARDS LOWER EMISSIONS

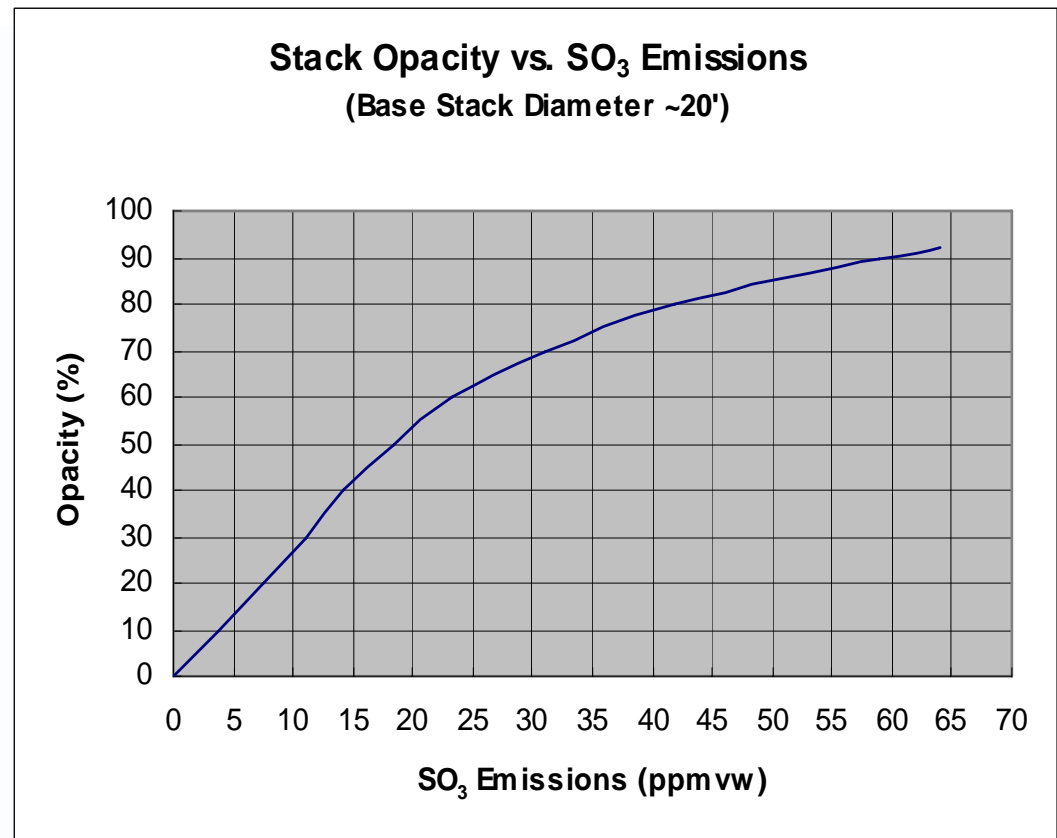


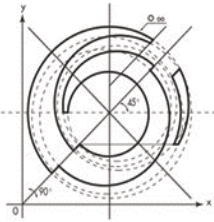
EMISSIONS REQUIREMENTS



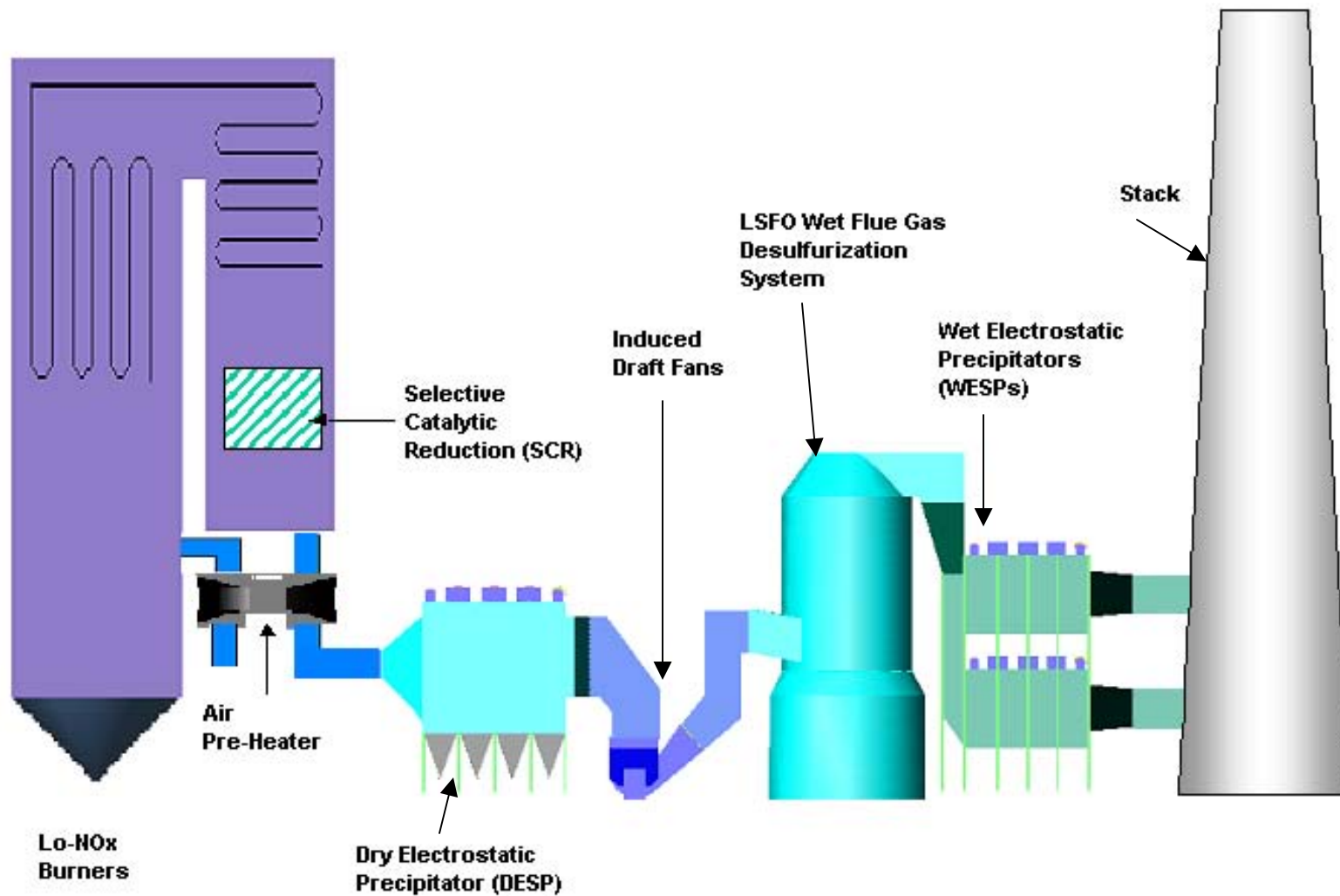
Trends:

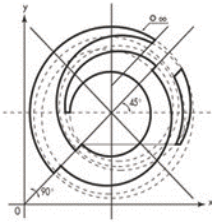
- Visible plume from stacks becoming an increasing concern
- Sub-micron particulate and SO_3 emissions are very visible
- Even with very low particulate emissions there may still be a plume associated with as little as 5 ppm of SO_3





Current Back-End APC Design





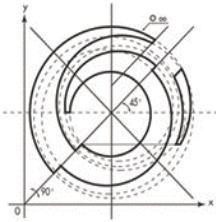
SO₃ Formation



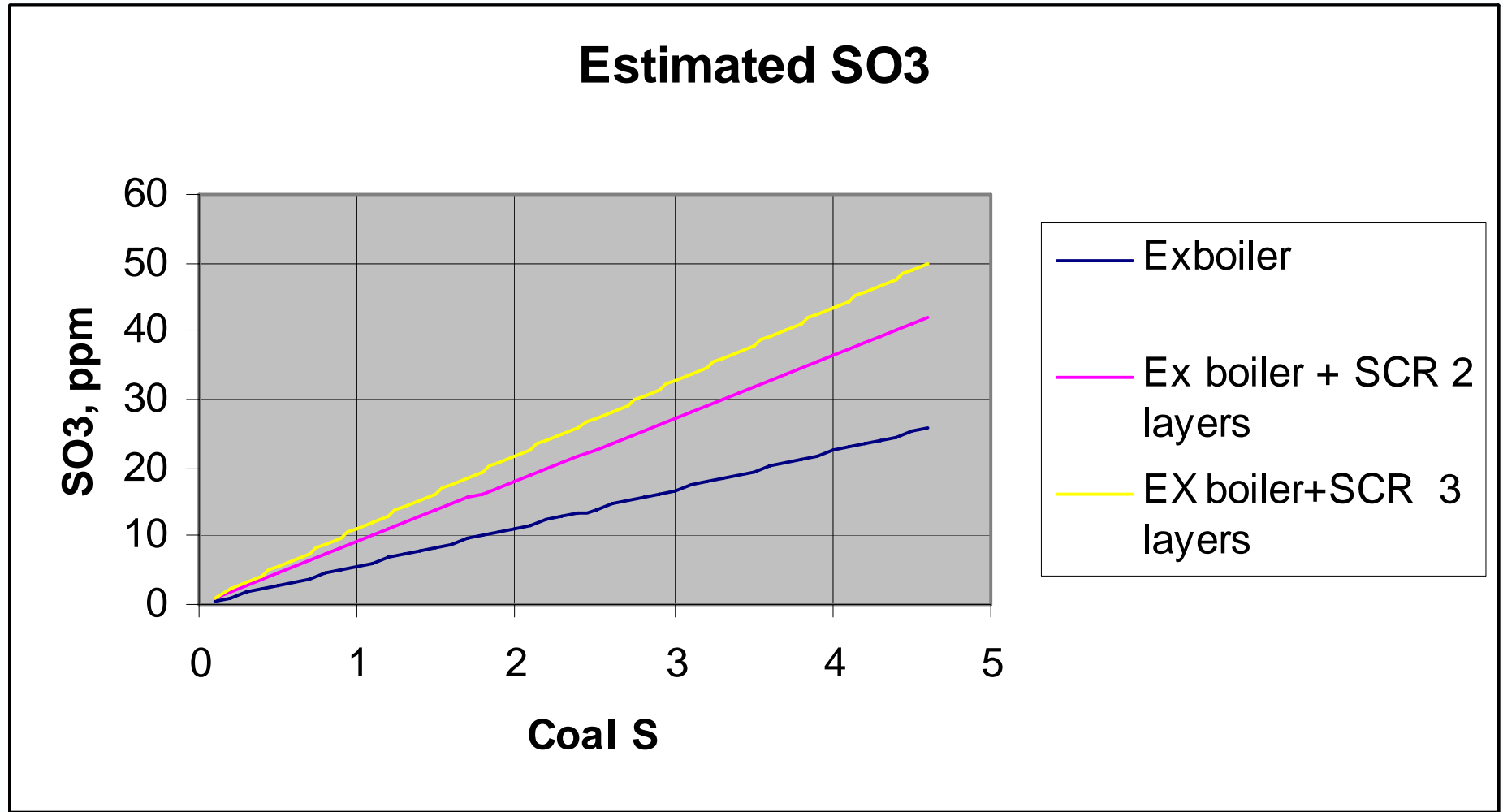
- Amount of oxidation in the boiler depends primarily on the coal composition and the excess air in firing
- Result is that $SO_3/SO_2 = 0.5\%/0.7\%$ at 10/30% excess air
- In practical engineering boiler engineers frequently use 1% flat figure, which most often probably is an **overestimate**
- A portion of the SO₃ is absorbed in the ash and in the APH
- SCR Catalyst manufacturer balances activity to get efficient NO_x reduction and limited SO₃ formation
- Typical SCR SO₃ formation is ~0.25 % oxidation per layer

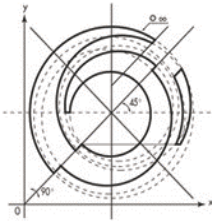
Coal S %	1	3
SO ₂ , ppm	600	1800
SO ₃ inlet SCR ppm	5	15
SO ₃ after 1st layer, ppm	6.5	19
SO ₃ after 2nd layer, ppm	8	24
SO ₃ after 3rd layer , ppm	10	30

- Low opacity requires <2-3 ppm SO₃ (drops) in the stack!

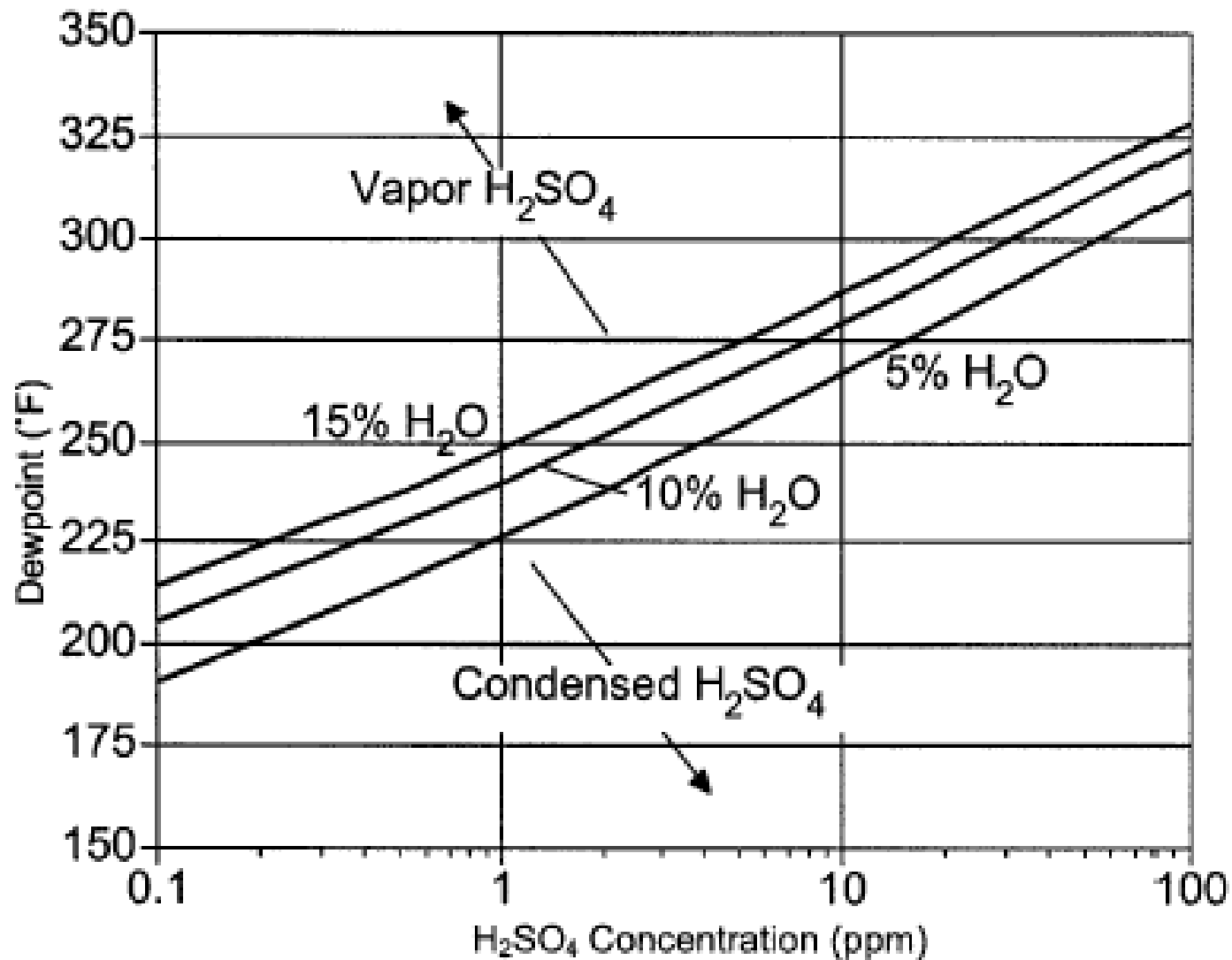


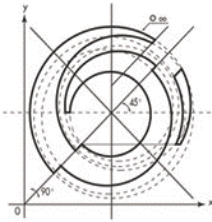
Estimated SO₃ for Different Coals



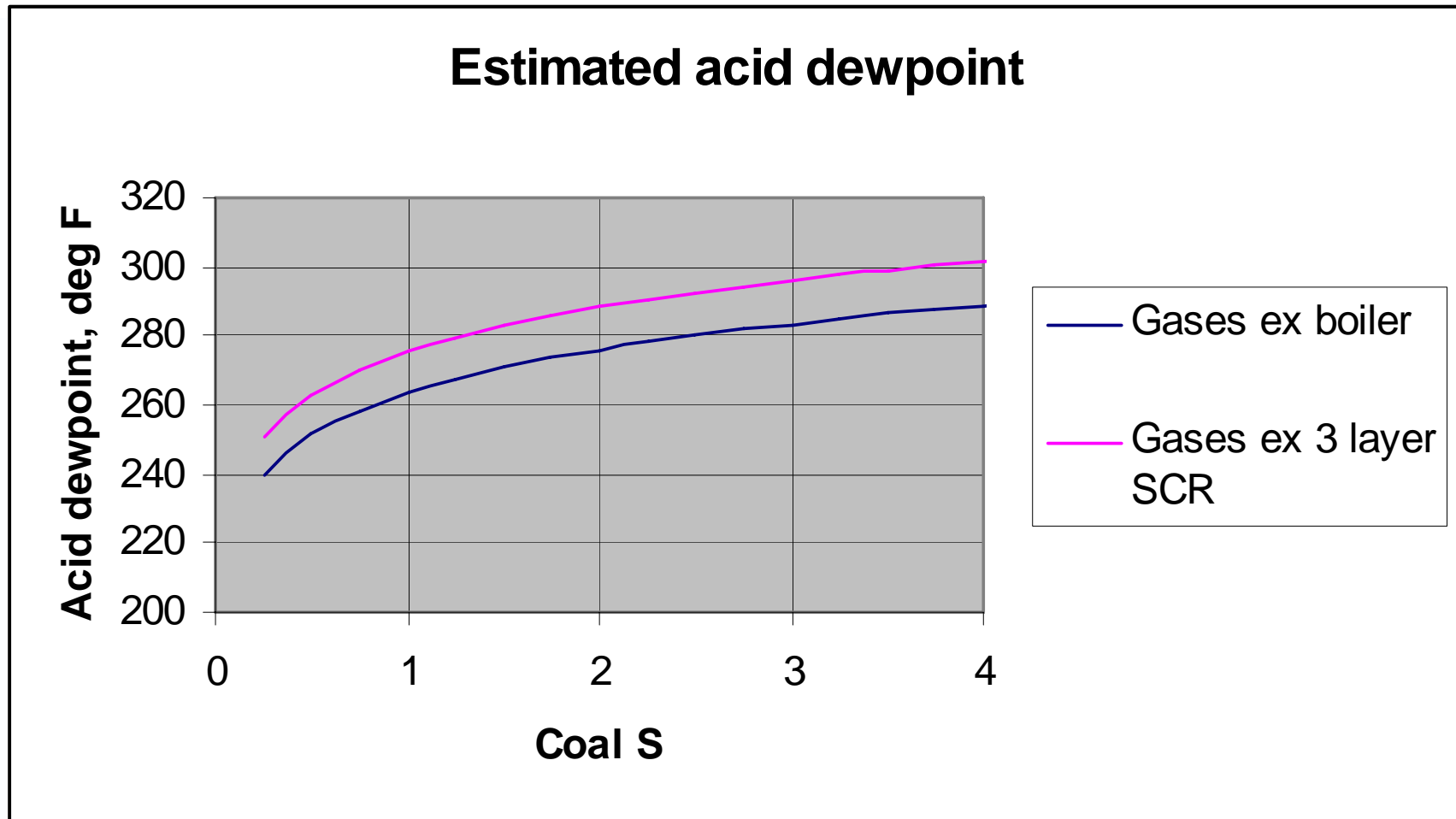


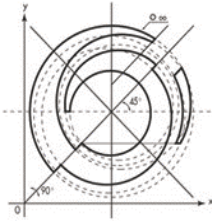
Acid Dewpoint





Estimated Dewpoint for Different Coals

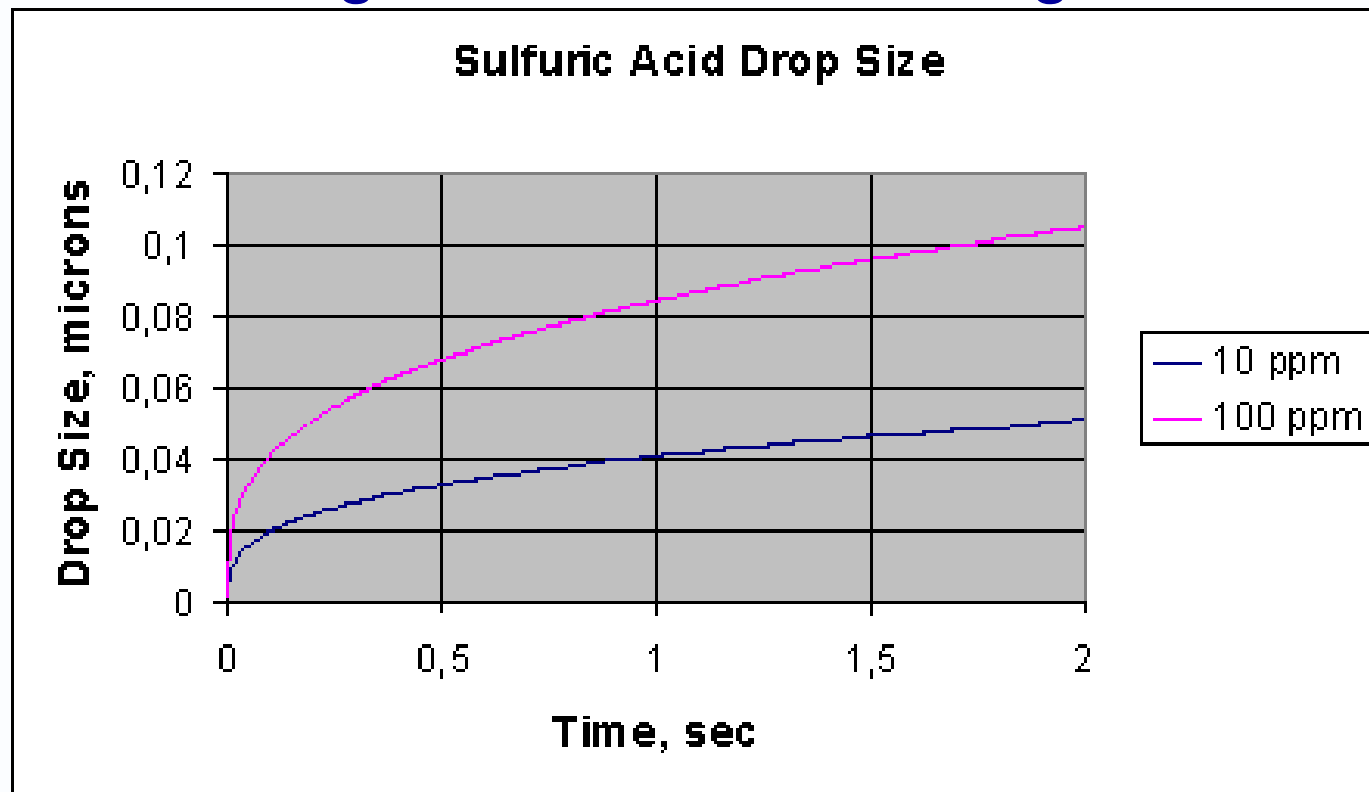


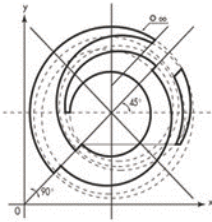


SO_3 (Actually it is H_2SO_4)

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- Cooling below acid dewpoint creates high supersaturation and creation of extremely fine H_2SO_4 mist, $0.05 \mu\text{m}$ size
- This fine mists grows as a result of coagulation:



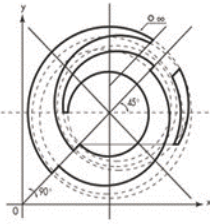


H_2SO_4 emitted from Open Spray Tower FGD

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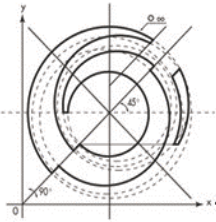
- Picture is from Cumberland, TN: 1300 MW SCR, ESP, WFGD, 3% S coal
- SO_2 efficiency=95% SO_3 efficiency=18%
- SO_3 emission of 15 ppm gives persistent plume after OST scrubber





Non-WESP Methods for SO₃ Control **ALSTOM**

1. Boiler injection : low utilization due to bad distribution & competition with SO₂. Impacts slagging & fouling in the boiler.
2. Ammonia injection downstream ESP. Works fine, low cost, but system produces stinking ash. Not an option for most systems due volume of ash problem.
3. Sorbent injection downstream of the economizer. Several chemical systems possible.
4. GGH together WFGD. Little experience (no high S in DE & JP where GGH's are used for other reasons).



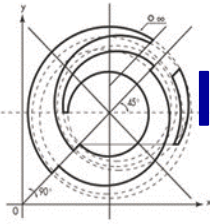
Sorbent Injection Performance



Consider SCR case , 3% S with SO_3 amounts (ppm).

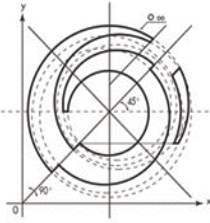
	Non-controlled	Controlled
After economizer	38	38
After ESP	33	4
After scrubber	16	2

Sorbent injection needs to achieve 90% efficiency to meet opacity goal!



Injection Methods for H_2SO_4 Control **ALSTOM**

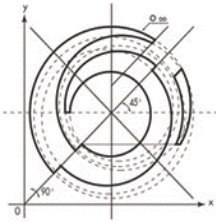
- **Low capital cost, corresponding tolerance for higher per lb operational cost**
- **The segment is $0.8\% < S < 1.5\%$ - WESP is selected for higher S**
- **Technical/ market candidate technologies:**
 - SBS patent by URS, injection of liquid upstream APH
 - Trona injection – patent by AEP
 - APH cooling + CaCO_3
 - $\text{Ca}(\text{OH})_2$ injection
 - MgO injection



Sorbent Injection: Issues/Concerns



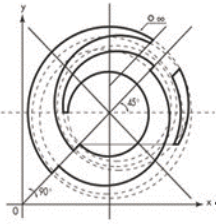
- Performance can be impacted by sorbent particle size and too short contact time
- Uniform injection of dry material in large ducts is a technical challenge
- Handling of some sorbent materials can be tricky
- Some sorbent materials can impact the nature of the ash such that ESP performance is reduced
- Some sorbent materials may impact the sale of the ash



GGH

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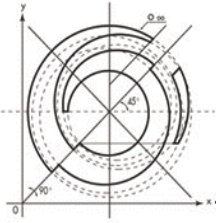
- GGH before/after scrubber reheats gas to 210 °F
- 1 ppm SO₃ (gas), 2 ppm SO₃ (drops) at stack
- 6 ppm upstream scrubber needed (scrubber efficiency 50%)
- GGH cooling side needs to reduce 80-85% from 33 ppm
May be possible.
- ALSTOM's experience from Niles (only known GGH on high S coal) is that yes, acid is indeed collected
- Effect not quantified
- Benchmark cost \$14/kW. Press drop 4" H₂O, capitalizes to about \$0.4/kW/yr. Spares and soot-blowing add to operating cost.
- GGH's not a proven solution for SO₃ control for opacity reduction on high S coals



Cost Comparison



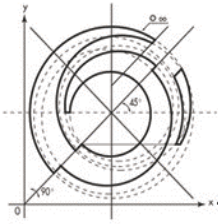
System	Capital \$/kW	Operation \$/kW/yr.	Notes
Ca(OH) ₂	2	3	Impacts ash
MgO	3	1.2	Estimated
SBS	5	0.75	Demonstrated
GGH	14	0.5	Available??
WESP	10-15	0.3	MgO neutr.



Why WESP?

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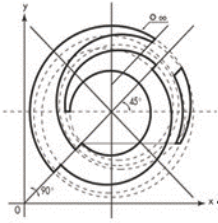
- Highest capital cost solution
- Added power consumption
- May impact plant H₂O usage
- Consumes valuable plant area
- Requires maintenance
- May require acid neutralization system (i.e. additional consumables)
- Requires significant time to integrate into plant operations



Why WESP?

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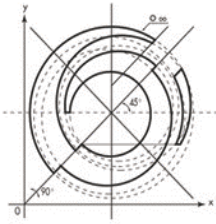
- **Many Installations in Japan**
 - Nakoso Power Station
 - Himeji Power Station
 - Shin-Nagoya Power Station
- **Existing units in NA with WESP's**
 - AES – Deepwater
 - Xcel Energy – Sherco Station
 - Dakota Gasification
 - New Brunswick Power – Dalhousie
 - New Brunswick Power – Coleson Cove



Why WESP?

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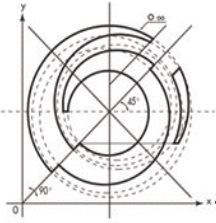
- **Active projects in NA including WESP's**
 - WE Energies Elm Road
 - EKP Spurlock Unit 1
 - EKP Spurlock Unit 2
 - Trimble County Unit 2
 - Dallman Power Station Unit 4



Why WESP?

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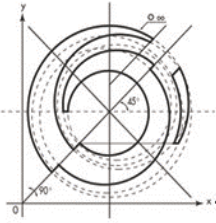
- **WESP's have been used for collection of H_2SO_4 Mist for nearly 100 years in industrial applications**
- **There is little doubt that they will effectively collect acid mist exhaust from coal fired boilers**
- **WESP's are excellent at collection of fine particulate**
 - Increased input power
 - Virtually no re-entrainment
 - Minimal pressure drop
- **The addition of a WESP does not create other problems in the APC system (such as impacting the ash properties)**



Addressing the Negatives



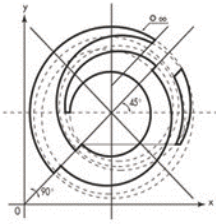
- **The high cost issues of WESP's are being addressed**
 - Lower conversion rate catalyst
 - Improved H_2SO_4 mist collection in the scrubber (Flowpac)
 - Larger size HF power supplies resulting in fewer bus sections
 - Lower cost alloy usage with the use of re-circulation system and acid neutralization system
- **The latest arrangement for the WESP's consumes less plant area – centralized water recirculation system**
- **Liquid blowdown from the WESP system used in the WFGD system**



WESP Advantages

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- **WESP's can collect more than acid mist and ash particulate matter**
 - Oxidized mercury
 - Sulfur dioxide
 - Hydrogen chloride
 - Hydrogen fluoride
 - HAP's such as arsenic, cadmium, chromium
- **The addition of a WESP provides added fuel flexibility**
 - Not as sensitive to variations in ash properties as dry ESP's
 - Dry ESP's work better with high S coals (lower resistivity)

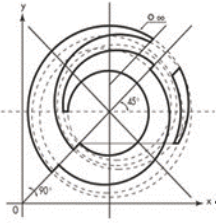


TYPES of WESP DESIGNS



WESP types available:

- **Vertical flow designs**
 - Round Tubes
 - Square Tubes
 - Rectangular Tubes
 - Hexagonal Tubes
 - Concentric Rings
 - Flat Plates
- **Horizontal flow flat plate type**
 - Rectangular casing
 - Round casing

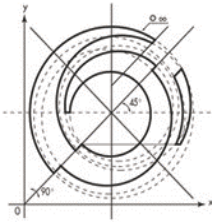


TYPES of WESP DESIGNS



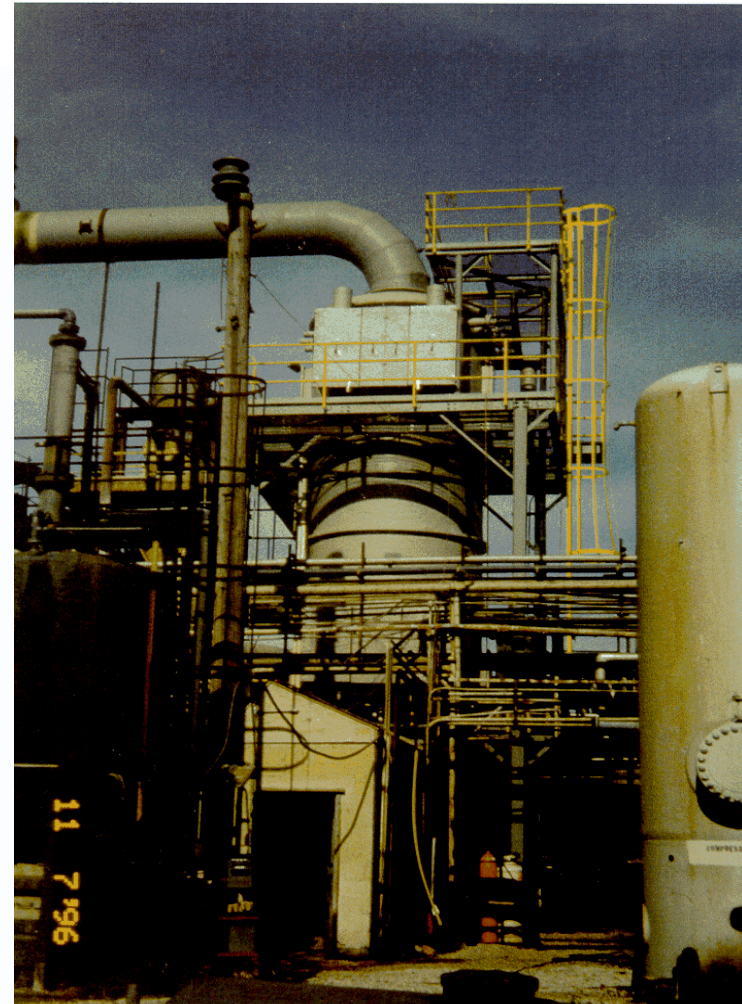
WESP configurations:

- **Vertical Flow Types - Non-Condensing**
No mechanical means are used to help precipitate the mist/liquid from the gas stream
- **Vertical Flow Types – Condensing WESP™ (Wheelabrator)**
Cool liquid is used to lower the temperature of the collecting surface to promote condensation of the warm, moist gas on the collector interior surface

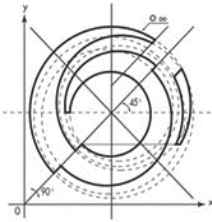


TYPES of WESP DESIGNS

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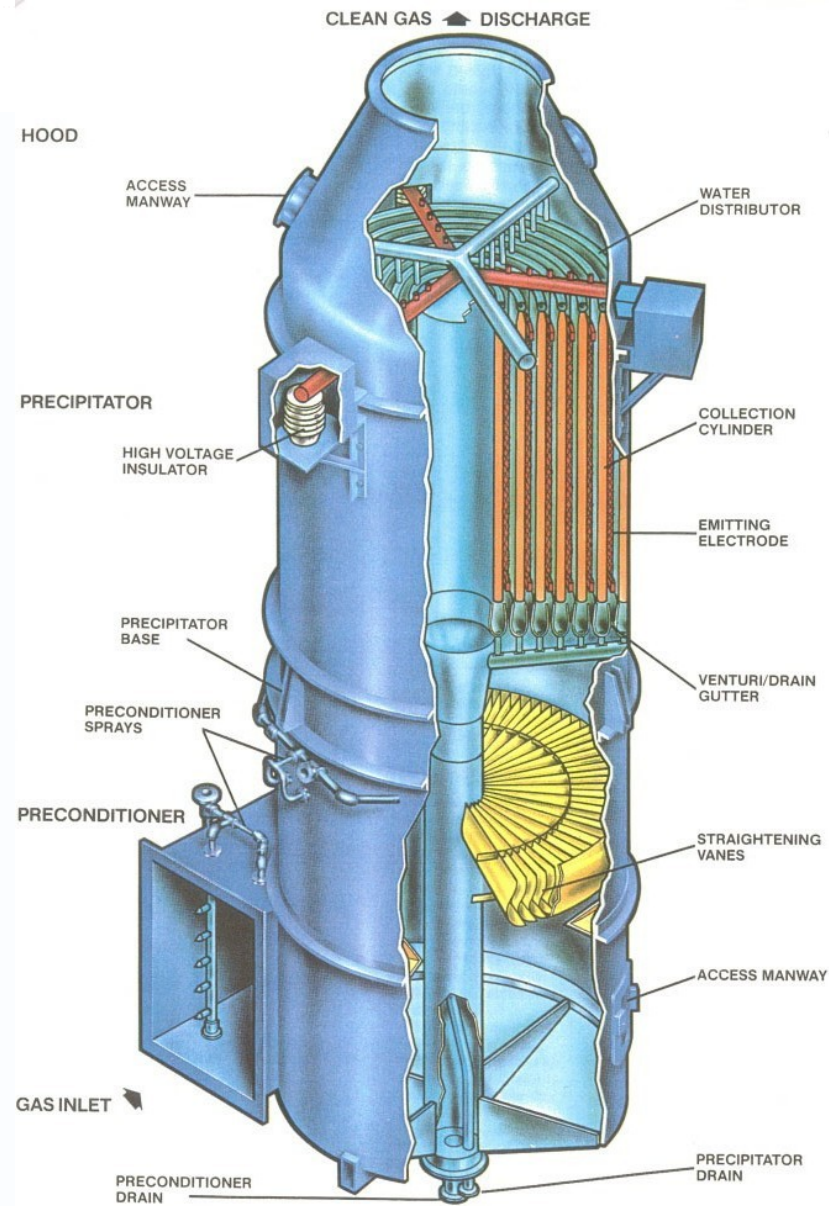
Old and New Style Tubular Vertical Flow WESP's

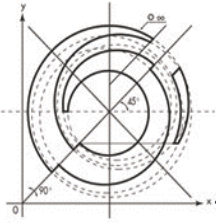


TYPES of WESP DESIGNS



Concentric Ring Style Vertical Flow WESP



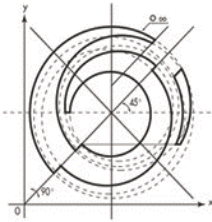


TYPES of WESP DESIGNS

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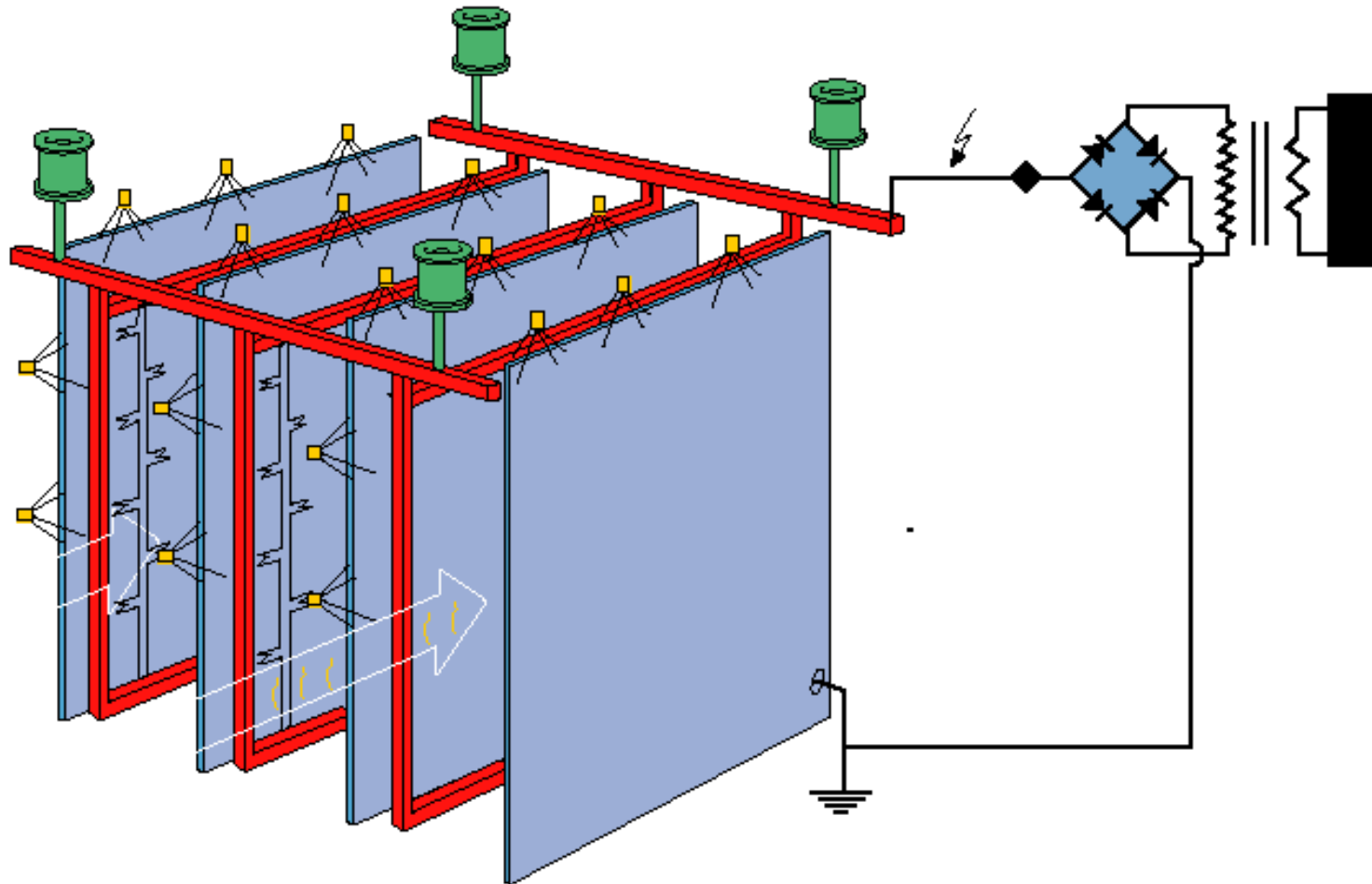
- **WESP configurations (continued):**
Horizontal Flow Designs:
 - Flat Plate Non-Irrigated* – No added liquid on the collecting surfaces - intermittent washing
 - Flat Plate Irrigated* – a stream of liquid covers the collecting surface to wash them clean
 - Flat Plate Flushed (washed)* – washing sprays are used continuously to clean the collecting and discharge electrodes

All Horizontal Flow Designs are: Non-Condensing Type

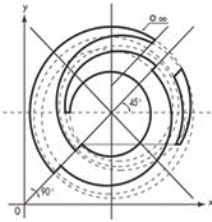


TYPES of WESP DESIGNS

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Basic Design of Horizontal Flow WESP with sprays
in front of and over the precipitation zone



WESP ARRANGEMENTS

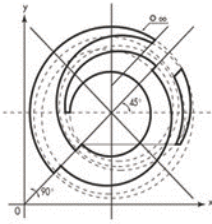


- **WESP Arrangements:**

- Multiple Vertical Flow Units in Parallel – to address large gas flows
- Multiple Vertical Flow Units in Series – to address high removal efficiencies
- Horizontal Flow Units with multiple cells and collecting fields in one casing to address large gas flows and high removal efficiencies

- **WESP's after WFGD Systems:**

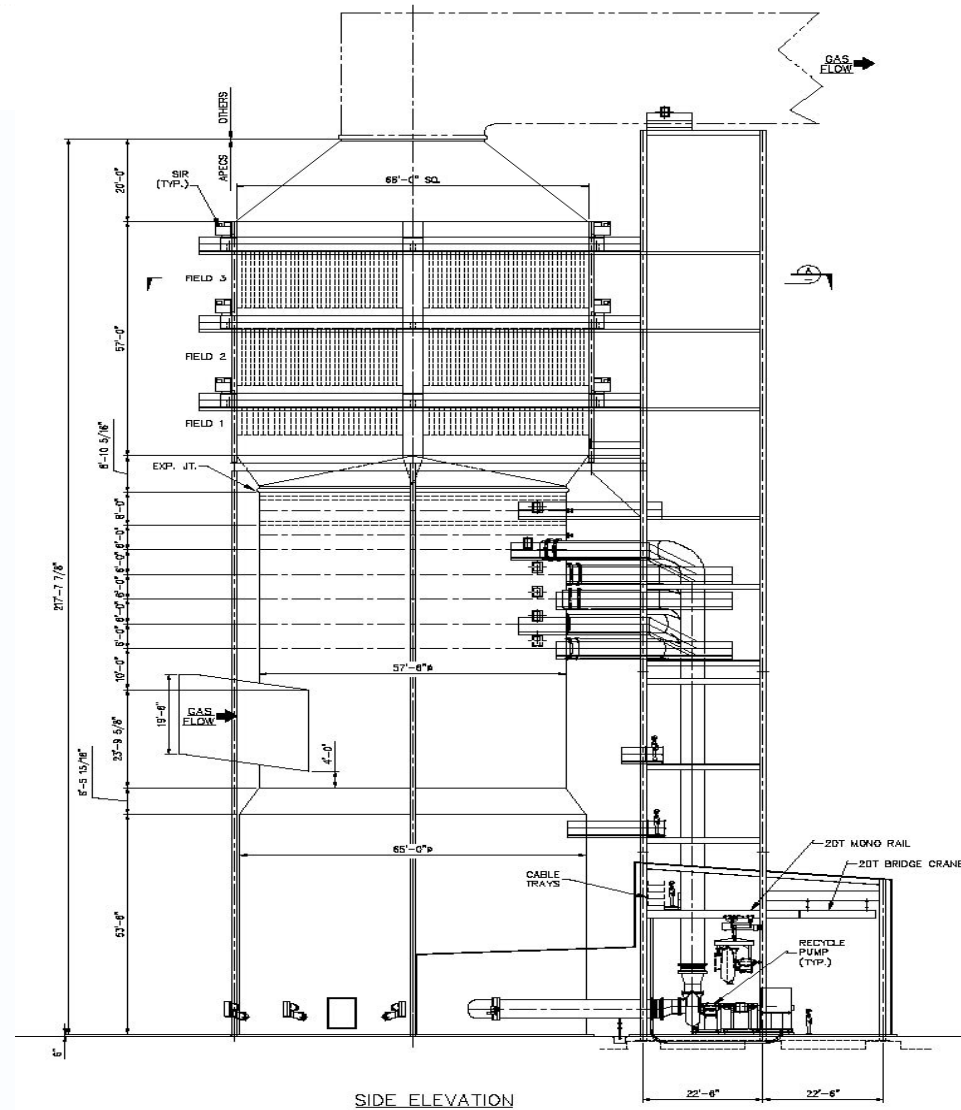
- Mounted in or on the top of the wet scrubber
- Grade mounted installations – VFWESP's
- Grade mounted installations – HFWESP's

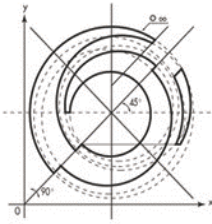


WESP ARRANGEMENTS



VFWESP In Scrubber Vessel Design

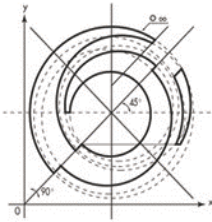




WESP ARRANGEMENTS



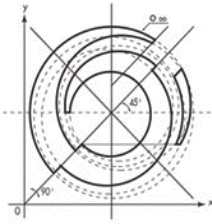
Tubular Vertical Flow WESP Arrangement



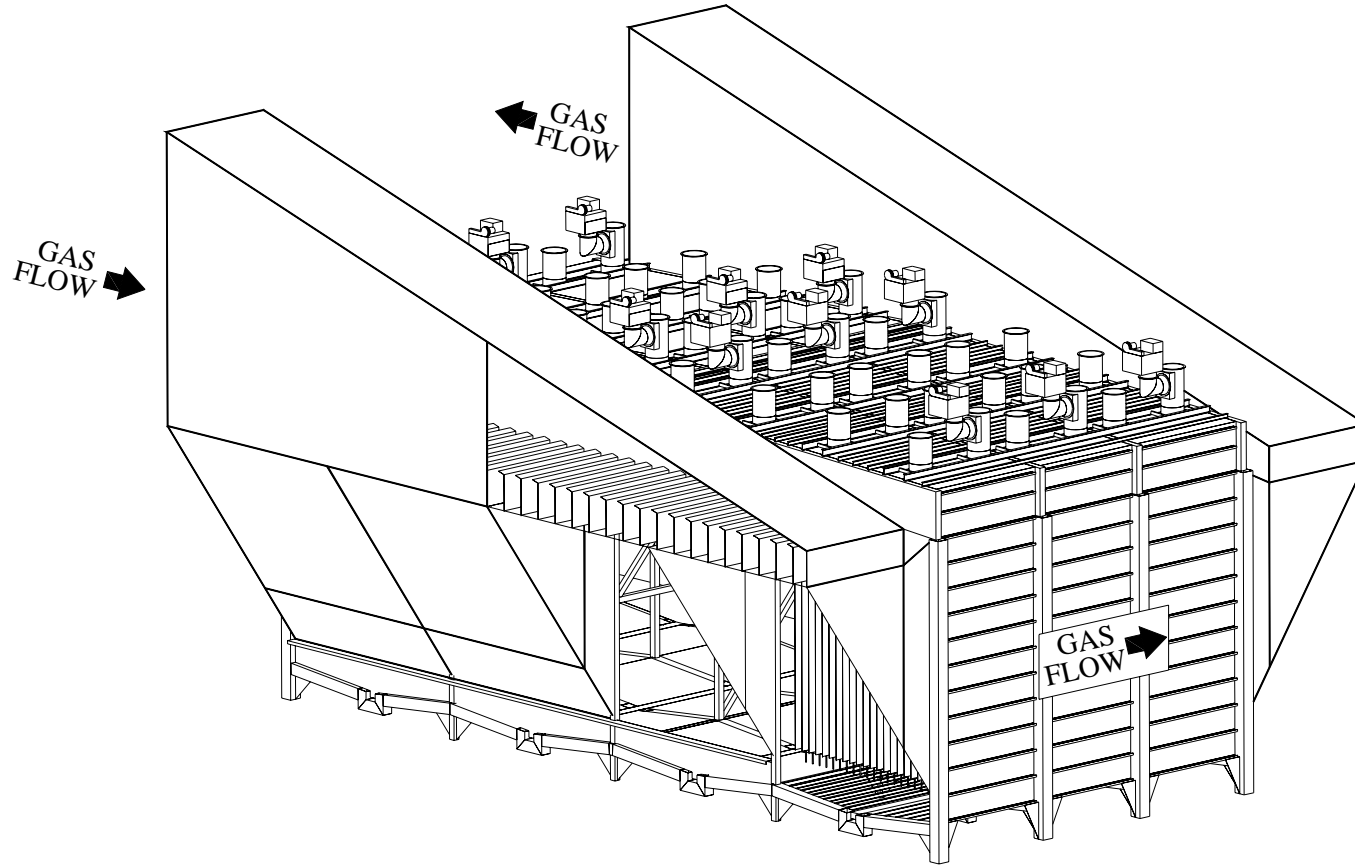
HFWESP DESIGN

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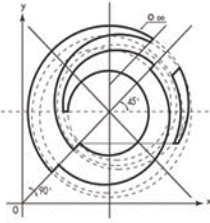
- Electrode spacing is 250 mm or 300 mm (10" or 12")
- Designed to meet conditions for WET environment with controlled water flow to reduce sparking
- Designed to reduce risk for corrosion including spray systems to keep all surfaces wet
- Maximum height of collecting plates is 9 meters (29.5')
- Discharge electrodes designed to increase current
- Wash water recirculation to reduce water consumption
- Design allows continuous flushing of internals



HORIZONTAL FLOW WESP DESIGN



Horizontal Flow WESP with multiple cells wide and multiple fields long in one casing



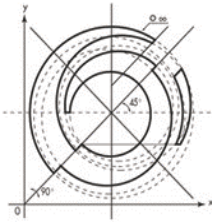
WESP MATERIALS of CONSTRUCTION



CHOICE OF MATERIALS DEPENDING ON PROCESS AND GAS COMPOSITION

MATERIAL is a major part of WESP cost

- Mild Steel
- Coated Mild Steel
- Wall Papered Mild Steel
- Fiberglass
- Corrosion Resistant Alloys.....



WESP MATERIALS



RISK FOR CORROSION

Alloy Materials

Material & fabrication/Lb

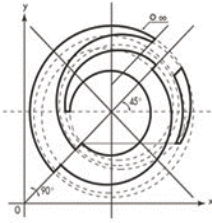
- 316L	\$3.50
- 2205	\$4.25
- 317LMN	\$5.00
- AL6XN	\$6.00
- 904L	\$6.00
- C276	\$16.00

MATERIAL



INCREASED COST

- Design to prevent corrosion
- Keep wash water at reasonable pH
- Control liquid chloride content
- Continuous flushing of all internals
- Keep ALL surfaces wet at all time

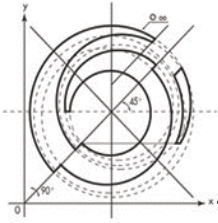


WESP INTERNALS CLEANING SYSTEMS

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CHOICE OF WASH WATER ARRANGEMENTS

- **Once through system**
 - Used on smaller size WESP systems
 - Used on low dust load systems
 - Most efficient cleaning system
 - Consumes large quantities of water
- **Re-circulation system**
 - Used on larger size WESP systems
 - Used on high dust load systems
 - Minimizes water consumption

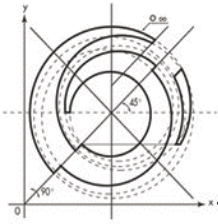


WESP INTERNALS CLEANING SYSTEMS

ALSTOM

WATER RE-CIRCULATION SYSTEM DESIGN

- **Complete contained systems provided**
 - Tanks
 - Pumps, piping and valves
 - Control system
- **Adjustable blow-down & make-up water**
 - Used to control % solids in re-circulation water
 - Used to control re-circulation water pH and chlorides content

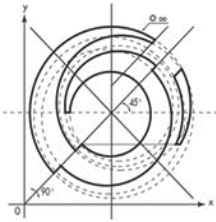


WESP INTERNALS CLEANING SYSTEMS

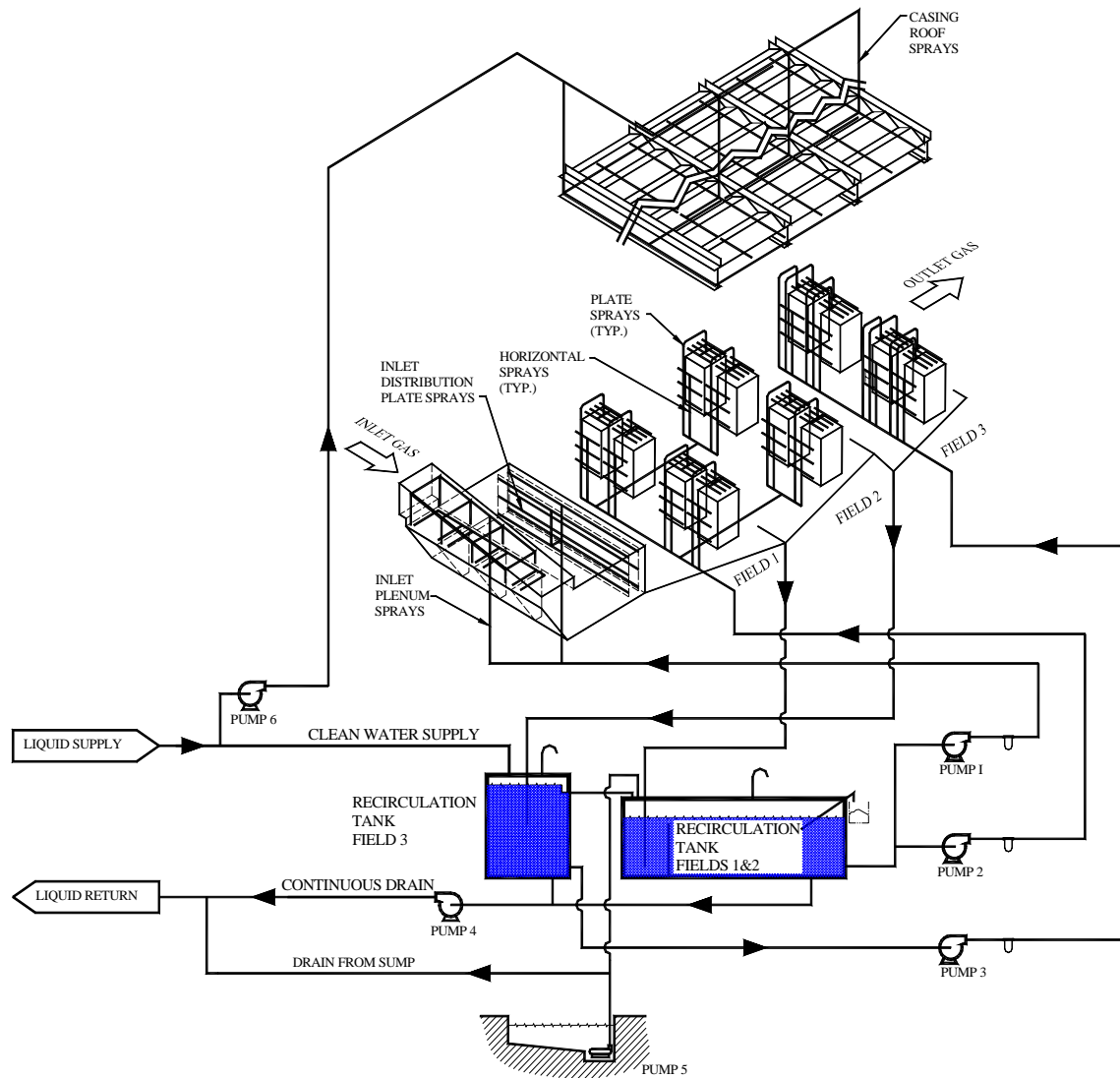


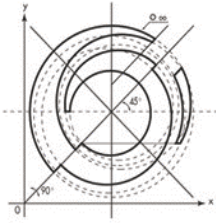
WATER RE-CIRCULATION SYSTEM DESIGN

- Segregated arrangement available if required
- Cleaner water in outlet
 - Lowers risk of dust carry-over
 - Lowers corrosion risk in outlet C.E. & D.E. fields
- Cleaner water for corrosion protection
 - Used to keep materials wet and flushed clean
 - Used to reduce casing/housing material corrosion risk



WESP INTERNALS CLEANING SYSTEMS

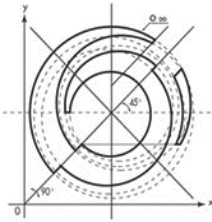




WESP SPRAY NOZZLE WASHING DESIGNS

ALSTOM

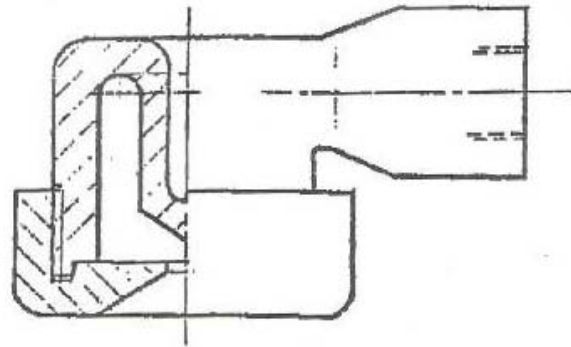
- Proprietary Centrifugal Nozzle
- Helix Spiral Nozzle
- Flat Jet Nozzle



WESP SPRAY NOZZLE WASHING DESIGNS

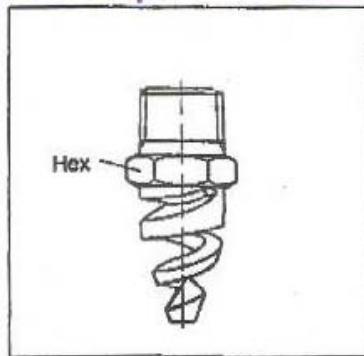


Centrifugal Nozzle ALSTOM Design



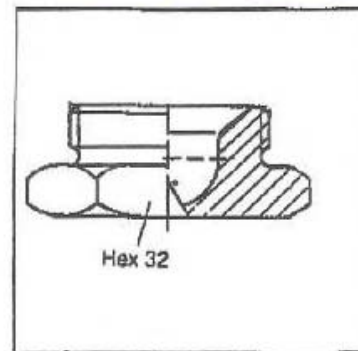
- HORIZONTAL SPRAYS
- VERTICAL PLATE SPRAYS

Helix Spiral Nozzle

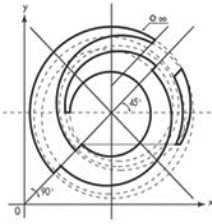


- HORIZONTAL SPRAYS

Flat Jet Nozzle



- VERTICAL PLATE SPRAYS

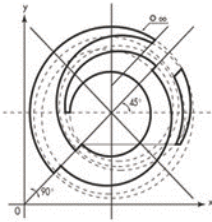


HFWESP WASH WATER SYSTEM



- **Horizontal flow wash water system**
 - Ensures completely saturated gas stream
 - Adds free moisture to gas stream that assists with precipitation and cleaning
 - May be operated continuously or intermittently

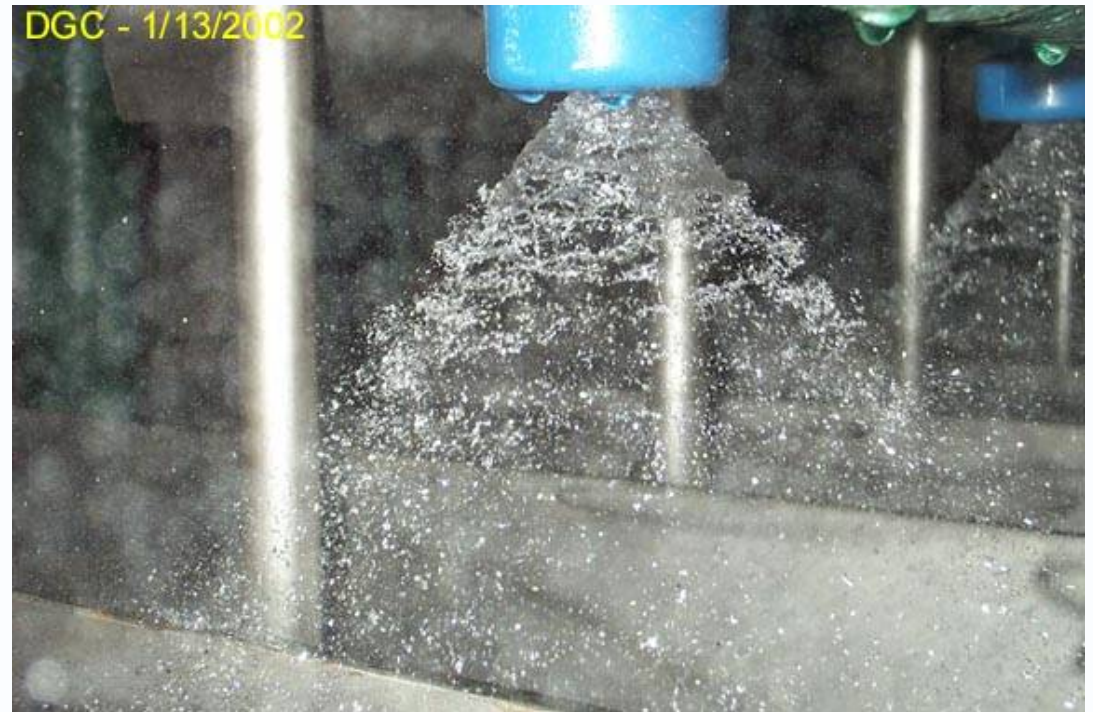


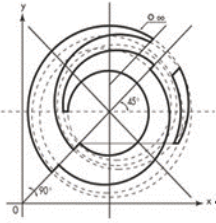


HFWESP WASH WATER SYSTEM



- **Top water sprays used to keep C.E.s clean**
 - Uniform flow of liquid over entire C.E. surface
 - Variable volume depending on process, typically 0.43 gpm/ft² or less
 - May be operated continuously or intermittently



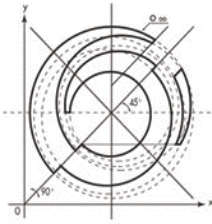


HFWESP INSTALLATIONS

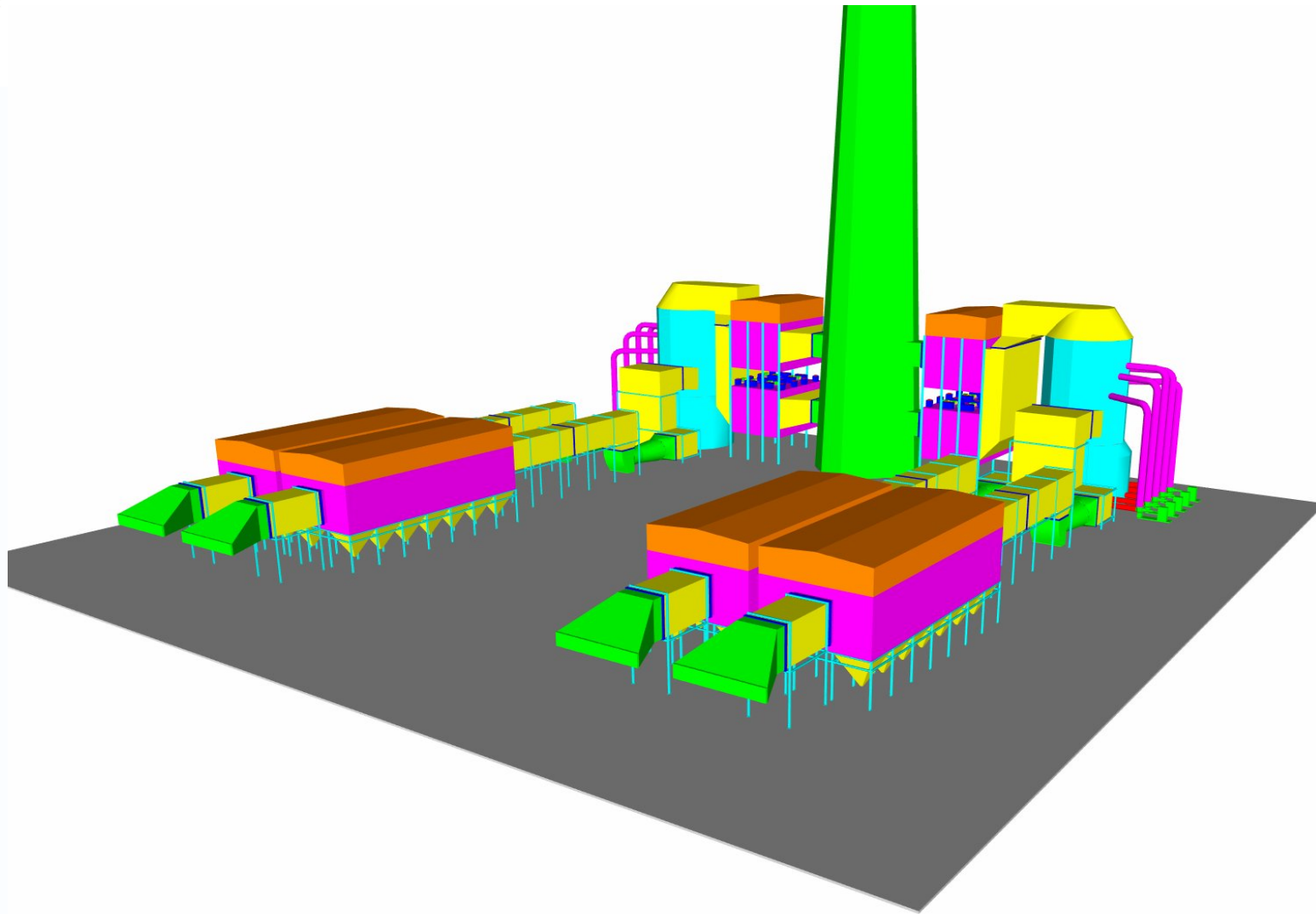


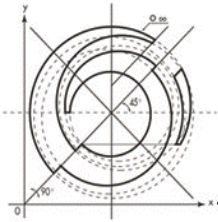
HFWESP REFERENCES

- **After coal fired boiler, ELM ROAD**
 - 650 MWe capacity system/boiler
 - Preceded by wet limestone scrubber
 - Design gas flow 720 Am³/s (1,530,000 ACFM)/boiler
 - 2 WESP's/boiler, 4 fields in series, 2 bus sections wide
 - Materials used 2205 and AL6XN
 - Gas velocity >2.46 m/s (>8.2 f.p.s.)
 - Outlet emissions: sized for 5.2 mg/Nm³ (0.0017 gr/scf)



APC System for Elm Road 2 X 650 MW ALSTOM

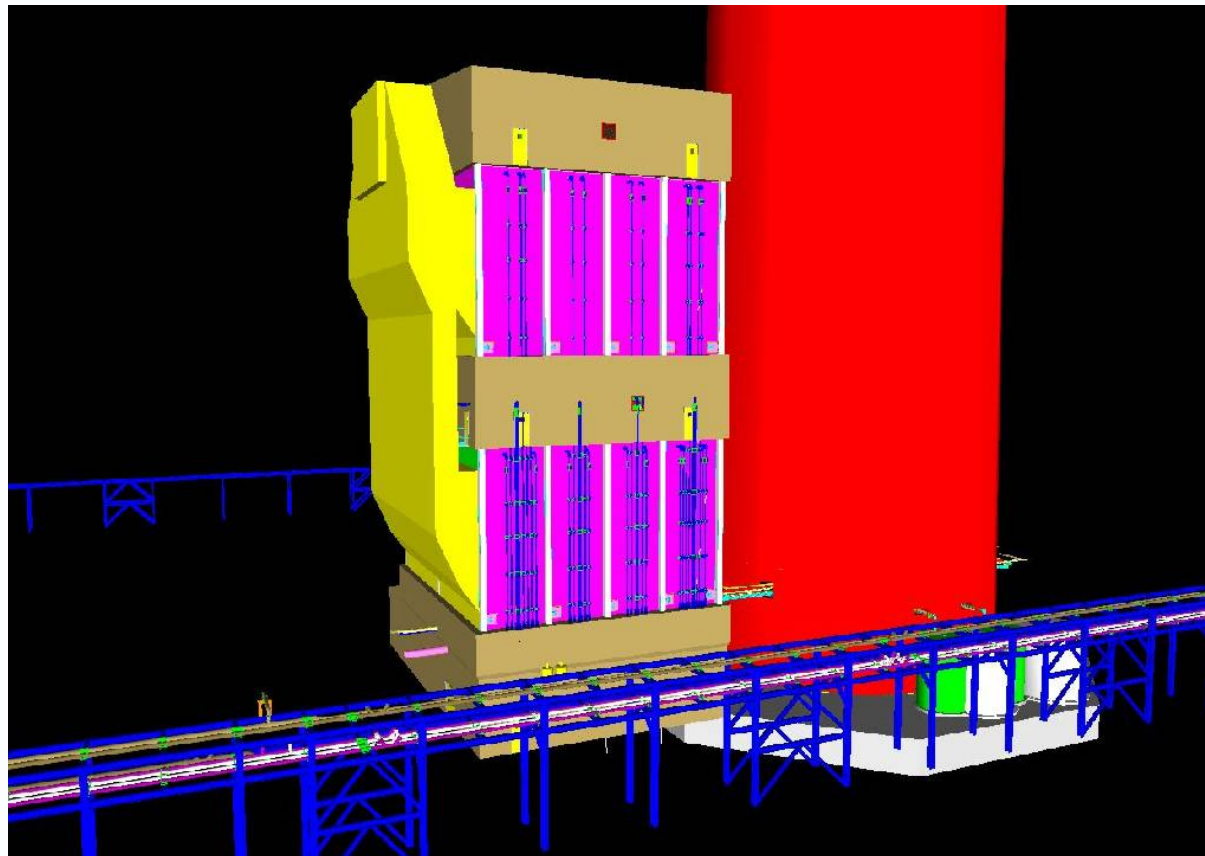


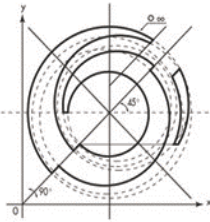


WET ESP



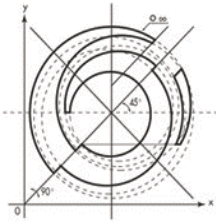
ELM ROAD, 2 WESP STACKED/BOILER





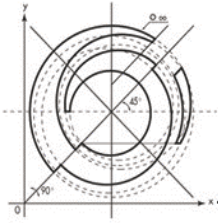
HFWESP MODULARIZATION





HFWESP INSTALLATIONS

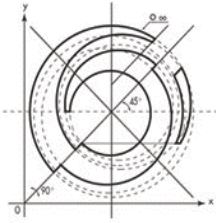




VFWESP INSTALLATIONS



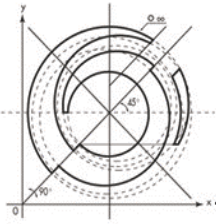
Grade Mounted Vertical Flow WESP System



VFWESP INSTALLATIONS



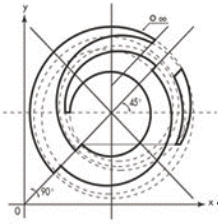
Vertical Flow WESP in WFGD



SUMMARY & CONCLUSIONS



- There exists an installed base of WESP's that provides excellent design knowledge for future projects
- WESP's have demonstrated excellent collection of sub-micron particulates, aerosols and fumes
- WESP's with multiple fields have demonstrated very high removal efficiencies
- WESP's may be arranged to suit site limitations
- HFWESP's, being very similar to DESP's in configuration, are ideal for use on high volume applications
- WESP's will collect condensed mercury and HAP's
- The use of a WESP system will not impact other APC equipment



CONCLUSION

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THANK YOU!

The image features the Alstom logo centered on a white semi-circular background. The logo consists of the word "ALSTOM" in a bold, sans-serif font. The letters "A", "L", "S", "T", and "M" are dark blue, while the letter "O" is red and stylized as a circle with a gap. A thick red arc curves over the top of the white background. The background behind the white arc is a dark blue field with vertical stripes of varying shades and some faint white curved lines.

ALSTOM

www.environment.power.alstom.com